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**EUROPEAN PATENT APPLICATION**

(21) Application number: 88300898.3

(22) Date of filing: 27.01.88

(81) Int. Cl.<sup>4</sup>: **C 08 F 4/64**  
**C 08 F 4/76, C 08 F 10/00,**  
**C 07 F 17/00**

(30) Priority: 30.01.87 US 11471 21.12.87- US 133052

(43) Date of publication of application:  
03.08.88 Bulletin 88/31

(84) Designated Contracting States:  
AT BE DE ES FR GB IT LU NL SE

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(54) Catalysts, method of preparing these catalysts, and polymerization processes wherein these catalysts are used.

(57) A catalyst is prepared by combining a bis(cyclopentadienyl)zirconium compound which may be represented by one of the following general formulae:

(A-Cp)MX<sub>1</sub>X<sub>2</sub>  
(A-Cp)MX<sub>1</sub>X'<sub>2</sub>  
(A-Cp)ML; and  
(Cp\*)(CpR)MX<sub>1</sub>

wherein:

M is a metal selected from the Group consisting of titanium (Ti), zirconium (Zr) and hafnium (Hf); (A-Cp) is either (Cp)(Cp\*) or Cp-A'-Cp\* and Cp and Cp\* are the same or different substituted or unsubstituted cyclopentadienyl radicals; A' is a covalent bridging group containing a Group IV-A element; L is an olefin, diolefin or aryne ligand; X<sub>1</sub> and X<sub>2</sub> are, independently, selected from the Group consisting of hydride radicals, hydrocarbyl radicals, substituted-hydrocarbyl radicals, organo-metalloid radicals and the like; X'<sub>1</sub> and X'<sub>2</sub> are joined and bound to the metal atom to form a metallocycle, in which the metal, X'<sub>1</sub> and X'<sub>2</sub> form a hydrocarbocyclic ring having from about 3 to about 20 carbon atoms; and R is a substituent on one of the cyclopentadienyl radicals which is also bound to the metal atom.

with a second compound comprising a cation capable of donating a proton and a bulky, labile anion comprising a plurality

of boron atoms capable of stabilizing the zirconium cation formally having a coordination number of 3 and a valence of +4 which is formed as a result of the combination, said second compound having one of the following general formulae:

$[L'-H] \{ [(CX)_a (BX')_m (X'')_b] \}^c$

Wherein:

L'-H is either H<sup>+</sup>, ammonium or a substituted-ammonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical, a phosphonium or substituted-phosphonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical and the like; B and C are, respectively, boron and carbon; X, X' and X'' are radicals selected, independently, from the Group consisting of hydride radicals, halide radicals, hydrocarbyl or substituted-hydrocarbyl radicals, organo-metalloid radicals and the like; a and b are integers  $\geq 0$ ; c is an integer  $\geq 1$ ; a + b + c = an even-numbered integer from 2 to about 8, and m is an integer ranging from 5 to about 22.

$[L'-H] \{ [(CX)_a (BX'_m) (X'_b) \}^c ]_2 Mn^+ \}^d$

Wherein:

L'-H is either H<sup>+</sup>, ammonium or a substituted-ammonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical, a phosphonium or substituted-phosphonium radical having up to 3 hydrogen

EP 0 277 003 A1

atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical and the like; B, C, M and H are, respectively, boron, carbon, a transition metal and hydrogen;  $X_3$ ,  $X_4$  and  $X_5$  are radicals selected, independently, from the Group consisting of hydride radicals, halide radicals, hydrocarbyl or substituted-hydrocarbyl radicals, organo-metalloid radicals and the like;  $a'$  and  $b'$  are the same or a different integer  $\geq 0$ ;  $c'$  is an integer  $\geq 2$ ;  $a' + b' + c' =$  an even-numbered Integer from 4 to about 8;  $m'$  is an integer from 6 to about 12;  $n$  is an integer such that  $2c' - n = d'$  and  $d'$  is an integer  $\geq 1$ .

Many of the catalysts thus formed are stable and isolable and may be recovered and stored. The catalysts may be preformed and then used to polymerize olefins or the catalysts may be formed in situ during polymerization by adding the separate components to the polymerization reaction. The catalysts will be formed when the two components are combined at a temperature within the range from about  $-100^\circ\text{C}$  to about  $300^\circ\text{C}$ . The catalysts thus prepared afford better control of polymer molecular weight and are not subject to equilibrium reversal. The catalysts thus produced are also less pyrophoric than the more conventional Ziegler-Natta olefin polymerization catalysts.

## Description

CATALYSTS, METHOD OF PREPARING THESE CATALYSTS, AND POLYMERIZATION PROCESSES  
WHEREIN THESE CATALYSTS ARE USED

This is a Continuation-in-Part of U.S. Patent Application Serial No. 011,471, filed January 30, 1987.

5 BACKGROUND OF THE INVENTION

This invention relates to compositions of matter useful as catalysts, to a method for preparing these catalysts, to a process wherein these compositions of matter are used as catalysts and to polymeric products produced with these catalysts. More particularly, this invention relates to catalyst compositions, to a method of making said catalyst compositions, to a method for polymerizing olefins, diolefins and/or acetylenically unsaturated monomers wherein these catalysts compositions are used, and to polymeric products produced with these catalyst compositions.

The use of soluble Ziegler-Natta type catalysts in the polymerization of olefins is, of course, well known in the prior art. In general, these soluble systems comprise a Group IV-B metal compound and a metal alkyl cocatalyst, particularly an aluminum alkyl cocatalyst. A subgenus of these catalysts is that subgenus comprising a bis(cyclopentadienyl) compound of the Group IV-B metals, particularly titanium, and an aluminum alkyl cocatalyst. While speculation remains concerning the actual structure of the active catalyst species in the subgenus of soluble Ziegler-Natta type olefin polymerization catalysts, it would appear generally accepted that the active catalyst species is an ion or a decomposition product thereof which will alkylate an olefin in the presence of a labile stabilizing anion. This theory may have first been advocated by Breslow and Newburg, and Long and Breslow, as indicated in their respective articles appearing in J. Am. Chem. Soc., 1959, Vol. 81, pp. 81-86, and J. Am. Chem. Soc., 1960, Vol. 82, pp. 1953-1957. As indicated in these articles, various studies suggested that the active catalyst species is a titanium-alkyl complex or a species derived therefrom when a titanium compound; viz., bis(cyclopentadienyl)titanium dihalide, and an aluminum alkyl are used as a catalyst or catalyst precursor. The presence of ions, all being in equilibrium, when a titanium compound is used was also suggested by Dyachkovskii, Vysokomol. Soed., 1965, Vol. 7, pp. 114-115 and by Dyachkovskii, Shilova and Shilov, J. Polym. Sci., Part C, 1967, pp. 2333-2339. That the active catalyst species is a cation complex when a titanium compound is used, was further suggested by Eisch et al., J. Am. Chem. Soc., 1985, Vol. 107, pp. 7219-7221.

While the foregoing articles teach or suggest that the active catalyst species is an ion pair and, particularly an ion pair wherein the metal component is present as a cation or a decomposition product thereof, and while these references teach or suggest coordination chemistry to form such active catalyst species, all of the articles teach the use of a cocatalyst comprising a Lewis acid either to form or to stabilize the active ionic catalyst species. The active catalyst is, apparently, formed through a Lewis acid-Lewis base reaction of two neutral components (the metallocene and the aluminum alkyl), leading to an equilibrium between a neutral, apparently inactive, adduct and an ion pair, presumably the active catalyst. As a result of this equilibrium, there is a competition for the anion which must be present to stabilize the active cation catalyst species. This equilibrium is, of course, reversible and such reversal will deactivate the catalyst. Moreover, the catalyst systems heretofore contemplated are subject to poisoning by the presence of basic impurities in the system. Further, many, if not all, of the Lewis acids heretofore contemplated for use in soluble Ziegler-Natta type catalyst systems are chain transfer agents and, as a result, prevent effective control of the product polymer molecular weight and product molecular weight distribution. Still further, most, if not all, of the cocatalysts heretofore contemplated are highly pyrophoric and, as a result, somewhat hazardous to use.

The aforementioned catalyst systems have not, generally, been particularly active when zirconium or hafnium is the Group IV-B metal used. Recently, however, it has been found that active Ziegler-Natta type catalysts can be formed when bis(cyclopentadienyl)hafnium and bis(cyclopentadienyl)zirconium compounds are used with alumoxanes. As is well known, these systems offer several distinct advantages, including vastly higher catalytic activities than the aforementioned bis(cyclopentadienyl)titanium catalysts and the production of polymers with narrower molecular weight distributions than those from conventional Ziegler-Natta catalysts. These systems remain subject to poisoning when basic impurities are present and do, however, require an undesirable excess of the alumoxane to function efficiently. Moreover, the hafnium containing systems are not as active as the zirconium containing systems, at least when used for homopolymerization. This has been suggested by Giannetti, Nicoletti, and Mazzocchi, J. Polym. Sci., Polym. Chem., 1985, Vol. 23, pp. 2117-2133, who claimed that the ethylene polymerization rates of bis(cyclopentadienyl)hafnium compounds were five to ten times slower than those of similar bis(cyclopentadienyl)zirconium compounds while there was little difference between the two catalysts in the molecular weight of the polyethylene formed from them.

In light of the several deficiencies of the coordination catalyst systems heretofore contemplated, the need for an improved coordination system which: (1) permits better control of molecular weight and molecular weight distribution; (2) is not subject to activation equilibrium; and (3) does not involve the use of an undesirable cocatalysts is believed readily apparent.

SUMMARY OF THE INVENTION

It has now been discovered that the foregoing and other disadvantages of the prior art ionic olefin polymerization catalysts can be avoided, or at least reduced, with the ionic catalysts of the present invention and an improved olefin, diolefin and/or acetylenically unsaturated monomer polymerization process provided therewith. It is, therefore, an object of this invention to provide improved ionic catalyst systems useful in the polymerization of olefins, diolefins and acetylenically unsaturated monomers. It is another object of this invention to provide a method for preparing such improved catalysts. It is a further object of this invention to provide an improved polymerization process using such improved catalysts. It is still another object of this invention to provide such an improved catalyst which is not subject to ion equilibrium reversal. It is still a further object of this invention to provide such an improved catalyst which may permit better control of the product polymer molecule weight and molecular weight distribution. It is yet a further object of this invention to provide such an improved catalyst which may be used with less risk of fire. It is even another object of this invention to provide polymeric products produced with these improved catalysts having relatively narrow molecular weight distributions and which are free of certain metal impurities. The foregoing and still other objects and advantages of the present invention will become apparent from the description set forth hereinafter and the examples included herein.

In accordance with the present invention, the foregoing and other objects and advantages are accomplished with and by using a catalyst prepared by combining at least two components, the first of which is a soluble, bis(cyclopentadienyl)-substituted Group IV-B metal compound containing at least one ligand which will combine with a Lewis or Bronsted acid thereby yielding a Group IV-B metal cation and the second of which compounds comprises a cation capable of donating a proton and reacting irreversibly with said ligand in said Group IV-B metal compound to liberate a free, neutral by-product and a compatible noncoordinating anion comprising a plurality of boron atoms, which compatible noncoordinating anion is stable, bulky and labile. The soluble Group IV-B metal compound must be capable of forming a cation formally having a coordination number of 3 and a valence of +4 when said ligand is liberated therefrom. The anion of the second compound must be capable of stabilizing the Group IV-B metal cation complex without interfering with the Group IV-B metal cation's or its decomposition product's ability to function as a catalyst and must be sufficiently labile to permit displacement by an olefin, a diolefin or an acetylenically unsaturated monomer during polymerization. For example, Bochmann and Wilson have reported (J. Chem. Soc., Chem. Comm., 1986, pp. 1610-1611) that bis(cyclopentadienyl)-titanium dimethyl reacts with tetrafluoroboric acid to form bis(cyclopentadienyl)titanium methyl tetrafluoroborate. The anion is, however, insufficiently labile to be displaced by ethylene.

DETAILED DESCRIPTION OF THE INVENTION

As indicated supra, the present invention relates to catalysts, to a method for preparing such catalysts, to a method of using such catalysts and to polymeric products produced with such catalysts. The catalysts are particularly useful in the polymerization of  $\alpha$ -olefins, diolefins and acetylenically unsaturated monomers. The improved catalysts are prepared by combining at least one first compound which is a bis(cyclopentadienyl) derivative of a metal of Group IV-B of the Periodic Table of the Elements capable of forming a cation formally having a coordination number of 3 and a valence of +4 and at least one second compound comprising a cation capable of donating a proton and a compatible noncoordinating anion comprising a plurality of boron atoms, which anion is both bulky and labile, and capable of stabilizing the Group IV-B metal cation without interfering with said Group IV-B metal cation's or its decomposition product's ability to polymerize  $\alpha$ -olefins, diolefins and/or acetylenically unsaturated monomers.

All reference to the Periodic Table of the Elements herein shall refer to the Periodic Table of the Elements, as published and copyrighted by CRC Press, Inc., 1984. Also, any reference to a Group or Groups of such Periodic Table of the Elements shall be to the Group or Groups as reflected in this Periodic Table of the Elements.

As used herein, the recitation "compatible noncoordinating anion" means an anion which either does not coordinate to said cation or which is only weakly coordinated to said cation thereby remaining sufficiently labile to be displaced by a neutral Lewis base. The recitation "compatible noncoordinating anion" specifically refers to an anion which when functioning as a stabilizing anion in the catalyst system of this invention does not transfer an anionic substituent or fragment thereof to said cation thereby forming a neutral four coordinate metallocene and a neutral boron by-product. Compatible anions are those which are not degraded to neutrality when the initially formed complex decomposes.

The Groups IV-B metal compounds, and particularly titanium, zirconium and hafnium compounds, useful as first compounds in the improved catalyst of this invention are bis(cyclopentadienyl) derivatives of titanium, zirconium and hafnium. In general, useful titanium, zirconium and hafnium compounds may be represented by the following general formulae:

1.  $(A-Cp)MX_1X_2$
2.  $(A-Cp)MX_1X'_2$
3.  $(A-Cp)ML$
4.  $(Cp^*)(CpR)MX_1$

wherein:

M is a metal selected from the Group consisting of titanium (Ti), zirconium (Zr) and hafnium (Hf); (A-Cp) is either (Cp)(Cp\*) or Cp-A'-Cp\* and Cp and Cp\* are the same or different substituted or unsubstituted

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hydrocarbyl radicals containing from 1 to about 20 carbon atoms, substituted-hydrocarbyl radicals, wherein one or more of the hydrogen atoms is replaced by a halogen atom, containing from 1 to about 20 carbon atoms, organo-metalloid radicals wherein each hydrocarbyl substitution in the organo portion or said organo-metalloid contains from 1 to about 20 carbon atoms and said metal is selected from Group IV-A of the Periodic Table of the Elements and the like;  $a'$  and  $b'$  are the same or a different integer  $\geq 0$ ;  $c'$  is an integer  $\geq 2$ ;  $a' + b' + c' =$  an even-numbered integer from 4 to about 8;  $m'$  is an integer from 6 to about 12;  $n$  is an integer such that  $2c' - n = d$ ; and  $d$  is an integer  $\geq 1$ .

Illustrative, but not limiting, examples of the second compounds which can be used as a second component in the catalyst compositions of this invention are ammonium salts such as ammonium 1-carbadodecaborate (using 1-carbadodecaborate as an illustrative, but not limiting, counterion for the ammonium cations listed below); monohydrocarbyl-substituted ammonium salts such as methylammonium 1-carbadodecaborate, ethylammonium 1-carbadodecaborate, propylammonium 1-carbadodecaborate, isopropylammonium 1-carbadodecaborate, (n-butyl)ammonium 1-carbadodecaborate, anilinium 1-carbadodecaborate, and (p-tolyl)ammonium 1-carbadodecaborate and the like; dihydrocarbyl-substituted ammonium salts such as dimethylammonium 1-carbadodecaborate, diethylammonium 1-carbadodecaborate, dipropylammonium 1-carbadodecaborate, diisopropylammonium 1-carbadodecaborate, di(n-butyl)ammonium 1-carbadodecaborate, diphenylammonium 1-carbadodecaborate, di(p-tolyl)ammonium 1-carbadodecaborate and the like; trihydrocarbyl-substituted ammonium salts such as trimethylammonium 1-carbadodecaborate, triethylammonium 1-carbadodecaborate, tripropylammonium 1-carbadodecaborate, tri(n-butyl) ammonium 1-carbadodecaborate, triphenylammonium 1-carbadodecaborate, tri(p-tolyl)ammonium 1-carbadodecaborate, N,N-dimethylanilinium 1-carbadodecaborate, N,N-diethylanilinium 1-carbadodecaborate and the like.

Illustrative, but not limiting examples of second compounds corresponding to Formula 5 [using tri(n-butyl)ammonium as an illustrative, but not limiting, counterion for the anions listed below] are salts of anions such as bis[tri(n-butyl)ammonium] nonaborate, bis[tri(n-butyl)ammonium]decaborate, bis[tri(n-butyl)ammonium]undecaborate, bis[tri(n-butyl)ammonium]dodecaborate, bis[tri(n-butyl)ammonium]decachlorodecaborate, bis[tri(n-butyl)ammonium]dodecachlorododecaborate, [tri(n-butyl)ammonium 1-carbadecaborate, tri(n-butyl)ammonium 1-carbaundecaborate, tri(n-butyl)ammonium 1-carbadodecaborate, tri(n-butyl)ammonium 1-trimethylsilyl-1-carbadecaborate, tri(n-butyl)ammonium dibromo-1-carbadodecaborate and the like; borane and carborane complexes and salts of borane and carborane anions such as decaborane(14), 7,8-dicarbaundecaborane(13), 2,7-dicarbaundecaborane(13), undecahydrido-7,8-dimethyl-7,8-dicarbaundecaborane, dodecahydrido-11-methyl-2,7-dicarbaundecaborane, tri(n-butyl)ammonium undecaborate(14), tri(n-butyl)ammonium 6-carbadecaborate(12), tri(n-butyl)ammonium 7-carbaundecaborate(13), tri(n-butyl)ammonium 7,8-dicarbaundecaborate(12), tri(n-butyl)ammonium 2,9-dicarbaundecaborate(12), tri(n-butyl)ammonium dodecahydrido-8-methyl-7,9-dicarbaundecaborate, tri(n-butyl)ammonium undecahydrido-8-ethyl-7,9-dicarbaundecaborate, tri(n-butyl)ammonium undecahydrido-8-butyl-7,9-dicarbaundecaborate, tri(n-butyl)ammonium undecahydrido-8-allyl-7,9-dicarbaundecaborate, tri(n-butyl)ammonium undecahydrido-9-trimethylsilyl-7,8-dicarbaundecaborate, tri(n-butyl)ammonium undecahydrido-4,6-dibromo-7-carbaundecaborate and the like; boranes and carboranes and salts of boranes and carboranes such as 4-carbanonaborane(14), 1,3-dicarbanonaborane(13), 6,9-dicarbaundecaborane(14), dodecahydrido-1-phenyl-1,3-dicarbanonaborane, dodecahydrido-1-methyl-1,3-dicarbanonaborane, undecahydrido-1,3-dimethyl-1,3-dicarbanonaborane and the like.

Illustrative, but not limiting, examples of second compounds corresponding to Formula 6 [using tri(n-butyl)ammonium as an illustrative, but not limiting, counterion for the anions listed below] are salts of metallacarborane and metallaborane anions such as tri(n-butyl)ammonium bis(nonahydrido-1,3-dicarbanonaborato) cobaltate(III), tri(n-butyl)ammonium bis(undecahydrido-7,8-dicarbaundecaborato)ferrate(III), tri(n-butyl)ammonium bis(undecahydrido-7,8-dicarbaundecaborato)cobaltate(III), tri(n-butyl) ammonium bis(undecahydrido-7,8-dicarbaundecaborato) nickelate(III), tri(n-butyl)ammonium bis(undecahydrido-7,8-dicarbaundecaborato) cuprate(III), tri(n-butyl)ammonium bis(undecahydrido-7,8-dicarbaundecaborato)aurate(III), tri(n-butyl)ammonium bis(nonahydrido-7,8-dimethyl-7,8-dicarbaundecaborato)ferrate(III), tri(n-butyl) ammonium bis(nonahydrido-7,8-dimethyl-7,8-dicarbaundecaborato) chromate(III), tris(n-butyl)ammonium bis(tribromooctahydrido-7,8-dicarbaundecaborato)cobaltate(III), tri(n-butyl)ammonium bis(dodecahydridodicarbadodecaborate)cobaltate(III), bis[tri(n-butyl)ammonium] bis(dodecahydridodecaborato) nickelate(II), tris[tri(n-butyl)ammonium] bis(undecahydrido-7-carbaundecaborato)chromate(III), bis[tri(n-butyl) ammonium] bis(undecahydrido-7-carbaundecaborato)manganate(IV), bis[tri(n-butyl)ammonium] bis(undecahydro-7-carbaundecaborato) cobaltate(III), bis[tri(n-butyl)ammonium] bis(undecahydrido-7-carbaundecaborato)nickelate(IV) and the like. A similar list of representative phosphonium compounds could be recited as illustrative second compounds, but for the sake of brevity, it is simply noted that the phosphonium and substituted-phosphonium salts corresponding to the listed ammonium and substituted-ammonium salts could be used as second compounds in the present invention.

In general, and while most first components identified above may be combined with most second components identified above to produce an active olefin polymerization catalyst, it is important to continued polymerization operations that either the initially formed metal cation or a decomposition product thereof be a relatively stable olefin polymerization catalyst. It is also important that the anion of the second compound be stable to hydrolysis when an ammonium salt is used. Further, it is important that the acidity of the second component be sufficient, relative to the first, to facilitate the needed proton transfer. Conversely, the basicity

of the metal complex must also be sufficient to facilitate the needed proton transfer. Certain metallocene compounds—using bis(pentamethylcyclopentadienyl)hafnium dimethyl as an illustrative, but not limiting example—are resistant to reaction with all but the strongest Bronsted acids and thus are not suitable as first components to form the catalysts described herein. In general, bis(cyclopentadienyl)metal compounds which can be hydrolyzed by aqueous solutions can be considered suitable as first components to form the catalysts described herein.

With respect to the combination of the desired cation and the stabilizing anion to form an active catalyst of the present invention, it should be noted that the two compounds combined for preparation of the active catalyst must be selected so as to ensure displacement of the anion by monomer or another neutral Lewis base. This could be done by steric hindrance, resulting from substitutions on the cyclopentadienyl carbon atoms as well as from substitutions on the anion itself. The use of perhydrocarbyl-substituted cyclopentadienyl metal compounds and/or bulky second components does not generally prevent the desired combination and, in fact, generally yields more labile anions. It follows, then, that metal compounds (first components) comprising perhydrocarbyl-substituted cyclopentadienyl radicals could be effectively used with a wider range of second compounds than could metal compounds (first components) comprising unsubstituted cyclopentadienyl radicals. In fact, first compounds comprising perhydrocarbyl-substituted cyclopentadienyl radicals would, generally, be effective when used in combination with second components having both larger and smaller anions. As the amount and size of the substitutions on the cyclopentadienyl radicals are reduced, however, more effective catalysts are obtained with second compounds containing larger anions, such as those encompassed by Equation 6 above and those having larger  $m$  values in Equation 5. In these cases, it is further preferable that in using second compounds which are encompassed by Equation 5,  $a + b + c = 2$ . Second compounds in which  $a + b + c =$  even-numbered integers of 4 or more have acidic B-H-B moieties which can react further with the metal cation formed, leading to catalytically inactive compounds.

In general, the catalyst can be prepared by combining the two components in a suitable solvent at a temperature within the range from about  $-100^{\circ}\text{C}$  to about  $300^{\circ}\text{C}$ . The catalyst may be used to polymerize  $\alpha$ -olefins and acetylenically unsaturated monomers having from two to about eighteen carbon atoms and diolefins having from four to about eighteen carbon atoms either alone or in combination. The catalyst may also be used to polymerize  $\alpha$ -olefins, diolefins and/or acetylenically unsaturated monomers in combination with other unsaturated monomers. In general, the polymerization will be accomplished at conditions well known in the prior art for the polymerization of monomers of this type. It will, of course, be appreciated that the catalyst system will form in situ if the components thereof are added directly to the polymerization process and a suitable solvent or diluent is used in said polymerization process. It is, however, preferred, to form the catalyst in a separate step prior to adding the same to the polymerization step. While the catalysts do not contain pyrophoric species, the catalyst components are sensitive to both moisture and oxygen and should be handled and transferred in an inert atmosphere such as nitrogen, argon or helium.

As indicated supra, the improved catalyst of the present invention will, generally, be prepared in a suitable solvent or diluent. Suitable solvents or diluents include any of the solvents known in the prior art to be useful as solvents in the polymerization of olefins. Suitable solvents, then, include, but are not necessarily limited to, straight and branched-chain hydrocarbons such as isobutane, butane, pentane, hexane, heptane, octane and the like, cyclic and alicyclic hydrocarbons such as cyclohexane, cyclopentane, methylcyclohexane, methylcycloheptane and the like and aromatic and alkyl substituted aromatic compounds such as benzene, toluene, xylene and the like. Suitable solvents also include basic solvents not heretofore useful as polymerization solvents when conventional Ziegler-Natta type polymerization catalysts are used such as chlorobenzene, dichloromethane and propyl chloride.

While the inventors do not wish to be bound by any particular theory, it is believed that when the two compounds used to prepare the improved catalysts of the present invention are combined in a suitable solvent or diluent, all or a part of the cation of the second compound (the proton) combines with one of the substituents on the metal-containing (first) component. In the case where the first component has a formula corresponding to that of general formula 1 supra, a neutral compound is liberated which either remains in solution or is liberated as a gas. In this regard, it should be noted that if the cation of the second compound is a proton and either  $X_1$  or  $X_2$  in the metal containing (first) compound is a hydride, hydrogen gas may be liberated. Similarly, if the cation of the second compound is a proton and either  $X_1$  or  $X_2$  is a methyl radical, methane may be liberated as a gas. In the cases where the first component has a formula corresponding to those of general formulae 2, 3 or 4, one of the substituents on the metal-containing (first) component is protonated but, in general, no substituent is liberated from the metal. It is preferred that the ratio of metal containing (first) component to second component cations be about 1:1 or greater. The conjugate base of the cation of the second compound, if such a portion does remain, will be a neutral compound which will remain in solution or complex with the metal cation formed, though, in general, a cation is chosen such that any binding of the neutral conjugate base to the metal cation will be weak or nonexistent. Thus, as the steric bulk of this conjugated base increases, it will, simply, remain in solution without interfering with the active catalyst. For example, if the cation of the second compound is an ammonium ion, this ion will liberate a hydrogen atom which may then react as in the case when the hydrogen atom was the cation to form gaseous hydrogen, methane or the like and the conjugate base of the cation will be ammonia. In like fashion, if the cation of the second compound were a hydrocarbyl-substituted ammonium ion containing at least one hydrogen atom, as is essential to the present invention, the hydrogen atom would be given up to react in the same fashion as when

hydrogen were the cation and the conjugate base of the cation would be an amine. Further, if the cation of the second compound were a hydrocarbyl-substituted phosphonium ion containing at least one proton, as is essential to the present invention, the conjugate base of the cation would be phosphine.

While still not wishing to be bound by any particular theory, it is also believed that when the metal containing (first) component has reacted with the second component, the non-coordinating anion originally contained in the second compound used in the catalyst preparation combines with and stabilizes either the metal cation, formally having a coordination number of 3 and a +4 valence, or a decomposition product thereof. The cation and anion will remain so combined until the catalyst is contacted with one or more olefins, diolefins and/or acetylenically unsaturated monomers either alone or in combination with one or more other monomers. As indicated supra, the anion contained in the second compound must be sufficiently labile to permit rapid displacement by an olefin, a diolefin or an acetylenically unsaturated monomer to facilitate polymerization.

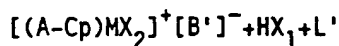
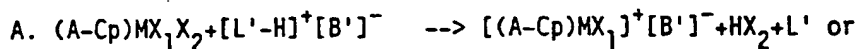
As indicated supra, most first compounds identified above will combined with most second compounds identified above to produce an active catalyst, particularly an active polymerization catalyst. The actual active catalyst species is not, however, always sufficiently stable as to permit its separation and subsequent identification. Moreover, and while many of the initial metal cations are relatively stable, it has become apparent that the initially formed metal cation may decompose yielding either an active polymerization catalyst species or a catalytically inactive species. Most decomposition products are, however, catalytically active. While the inventors still do not wish to be bound by any particular theory, it is believed that the active catalyst species which have not been isolated, including active decomposition products, are of the same type as those which have been isolated and fully characterized or at least retain the essential structure required for functioning as a catalyst such as a reactive metal-carbon bond.

While still not wishing to be bound by any particular theory and as indicated supra, it is also believed that the extent and nature of the substitution on the cyclopentadienyl ring dictates the size of the stabilizing anion needed to generate a particularly active olefin polymerization catalyst. In this regard, it is believed that as the number of substituents on the cyclopentadienyl radical in the metallocene cation are decreased from 5 to 0, a given anion will become increasingly less labile. Thus, it is suggested that as the number of substituents on the cyclopentadienyl radical in the metallocene cation are reduced from 5 to 0, larger or less reactive anions should be used to ensure lability and allow for the generation of a particularly active catalyst species.

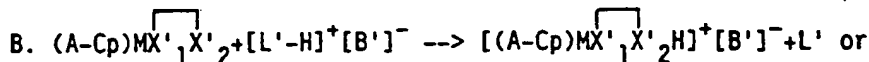
Consistent with the foregoing, stable, isolable, characterizable olefin polymerization catalysts have been prepared when bis(permethylocyclopentadienyl)zirconium dimethyl has been combined with and reacted with tri(n-butyl)ammonium 7,8-dicarbaundecaborate(12) or 7,8-dicarbaundecaborane(13). A stable, isolable, olefin polymerization catalyst has also been prepared when bis(ethyltetramethylocyclopentadienyl)zirconium dimethyl has been combined with 7,8-dicarbaundecaborane(13). In each of these cases, the stable polymerization catalyst was prepared by adding the reactants into a suitable solvent or diluent at a temperature within the range from about -100°C to about 300°C. Based on this and other information available to the inventors, it appears clear that isolable and characterizable polymerization catalysts can also be prepared when a bis(perhydrocarbyl-substituted cyclopentadienyl)metal compound is combined with any one or more of the second compounds identified above. Also, active, but unisolated polymerization catalysts are prepared when bis(cyclopentadienyl)zirconium compounds containing less than five hydrocarbyl-substitutions on each cyclopentadienyl radical are reacted with a suitable second compound, within the scope of the present invention, containing a cation capable of donating a proton and an anion capable of stabilizing the metallocene cation and sufficiently labile to be displaced by an olefin, a diolefin or an acetylenically unsaturated monomer during polymerization, particularly those second compounds having the larger anions.

The chemical reactions which occur may be represented by reference to the general formulae set forth herein as follows:

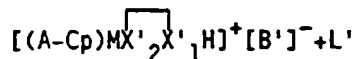




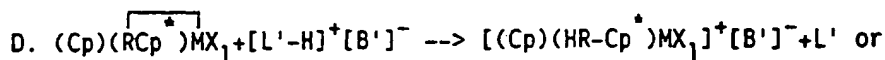
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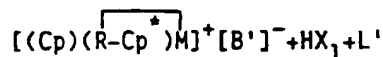
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In the foregoing reaction equations, the letters A-D correspond to the numbers 1-4, respectively, set forth in combination with the general equations for useful metallocene compounds. B' represents a compatible ion corresponding to the general formulae outlined in formulae 5 and 6 above. The reaction of each of the four classes of metallocenes with N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III) has been examined by solution <sup>1</sup>H NMR or <sup>13</sup>C NMR spectroscopy. In each case, products conforming to those outlined above were observed.

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In general, the stable, isolable catalysts formed by the method of this invention may be separated from the solvent and stored for subsequent use. The unisolated catalysts, however, will, generally, be retained in solution until ultimately used in the polymerization of olefins. Alternatively, any of the catalysts prepared by the method of this invention may be retained in solution for subsequent use or used directly after preparation as a polymerization catalyst. Moreover, and as indicated supra, the catalysts may be prepared in situ by passing the separate components into the polymerization vessel where the components will be contacted and react to produce the improved catalyst of this invention.

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In general, and as indicated supra, the improved catalyst of this invention will polymerize olefins, diolefins and/or acetylenically unsaturated monomers either alone or in combination with other olefins and/or other unsaturated monomers at conditions well known in the prior art for conventional Ziegler-Natta catalysis. In the polymerization process of this invention, the molecular weight appears to be a function of both catalyst concentration, polymerization temperature and polymerization pressure. In general, the polymers produced with the catalyst of this invention, when produced in an atmosphere free of hydrogen or other chain terminating agents, will contain terminal unsaturation.

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The polymer products produced with the catalyst of this invention will, of course, be free of certain trace metals generally found in polymers produced in Ziegler-Natta type catalysts such as aluminum, magnesium, chloride and the like. The polymer products produced with the catalysts of this invention should then have broader range of applications than polymers produced with more conventional Ziegler-Natta type catalysts comprising a metal alkyl, such as an aluminum alkyl.

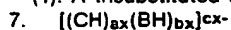
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#### PREFERRED EMBODIMENT OF THE INVENTION

In a preferred embodiment of the present invention, a polymerization catalyst will be prepared by combining a bis(cyclopentadienyl) compound of one of the Group IV-B metals, most preferably a bis(cyclopentadienyl)zirconium or bis(cyclopentadienyl)hafnium compound, containing two independently substituted or unsubstituted cyclopentadienyl radicals and two lower alkyl substituents or two hydrides with one of the following:

55

(1). A trisubstituted ammonium salt of a borane or carborane anion satisfying the general formula:



60

Wherein:

B, C, and H are, respectively, boron, carbon and hydrogen;

ax is either 0 or 1; cx is either 1 or 2; ax + cx = 2; and

bx is an integer ranging from 10 to 12.

(2). A trisubstituted ammonium salt of a borane or carborane anion or a neutral borane or carborane

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compound satisfying the general formula:

8.  $[(CH)_{ay}(BH)_{my}H_{by}]^{cy-}$

wherein:

B, C and H are, respectively, boron, carbon and hydrogen;

5  $ay$  is an integer from 0 to 2;  $by$  is an integer from 0 to 3;

$cy$  is an integer from 0 to 3;  $ay + by = cy = 4$ ; and  $my$  is an integer from 9 to 18.

(3). A trisubstituted ammonium salt of a metallaborane or metallocarborane anion satisfying the general formula:

9.  $[[[(CH)_{az}(BH)_{mz}H_{bz}]^{cz-}]_2MZ^{nz+}]^{dz-}$

10 Wherein:

B, C, H and MZ are, respectively, boron, carbon, hydrogen and a transition metal;  $az$  is an integer from 0 to 2;

$bz$  is an integer from 0 to 2;  $cz$  is either 2 or 3;

$mz$  is an integer from 9 to 11;  $az + bz + cz = 4$ ; and  $nz$  and  $dz$  are, respectively, 2 & 2 or 3 & 1.

Each of the trisubstitutions in the ammonium cation will be the same or a different lower alkyl or aryl radical. By lower alkyl is meant an alkyl radical containing from one to four carbon atoms. In a most preferred embodiment of the present invention wherein an anion represented by Formula 7 is used, bis(pentamethylcyclopentadienyl)zirconium dimethyl will be combined with tri(n-butyl)ammonium 1-carbaundecaborate to produce a most preferred catalyst. In a most preferred embodiment of the present invention wherein an anion represented by Formula 8 is used, bis(pentamethylcyclopentadienyl)zirconium dimethyl will be combined with 7,8-dicarbaundecaborane(13) to produce a most preferred catalyst. In a most preferred embodiment of the present invention wherein an anion represented by Formula 9 is used, bis(cyclopentadienyl)zirconium or -hafnium dimethyl will be combined with N,N-dimethylaluminum bis(7,8-dicarbaundecaborato) cobaltate(III) to produce a most preferred catalyst. In a preferred embodiment of this invention, the two components used to prepare the catalyst will be combined at a temperature within the range from about 0°C to about 100°C. The components will be combined, preferably, in an aromatic hydrogen solvent, most preferably toluene. Nominal holding times within the range from about 10 seconds to about 60 minutes will be sufficient to produce both the preferred and most preferred catalysts of this invention.

In a preferred and most preferred embodiment of this invention, the catalyst, immediately after formation, will be used to polymerize one or more lower  $\alpha$ -olefins, particularly ethylene and propylene, most preferably ethylene, at a temperature within the range from about 0°C to about 100°C and at a pressure within the range from about 15 to about 500 psig. The monomers will be maintained at polymerization conditions for a nominal holding time within the range from about 1 to about 60 minutes and the catalyst will be used at a concentration within the range of about  $10^{-6}$  to about  $10^{-1}$  moles per liter of solvent or diluent.

Having thus broadly described the present invention and a preferred and most preferred embodiment thereof, it is believed that the same will become even more apparent by reference to the following examples. It will be appreciated, however, that the examples are presented solely for purposes of illustration and should not be construed as limiting the invention. In the examples wherein an active catalyst was isolated and identified, the analysis was by solid-state  $^{13}C$  NMR spectroscopy and solution  $^1H$  NMR spectroscopy.

#### 40 EXAMPLE 1

In this example, an active olefin polymerization catalyst was prepared and isolated by combining 1.0 g of bis(pentamethylcyclopentadienyl)zirconium dimethyl in 50 ml of toluene and then adding 0.82 g of tri(n-butyl)ammonium 7,8-dicarbaundecaborate(12). The mixture was stirred at room temperature for 30 minutes, the solvent was evaporated to half its original volume and pentane added to the point of cloudiness. After cooling at -20°C overnight, a yellow solid was filtered off, washed with pentane and dried. The yield of active catalyst was 0.75 g. A portion of this product was analyzed and identified as bis(pentamethylcyclopentadienyl)(dodecahydrido-7,8-dicarbaundecaborato)zirconium.

#### EXAMPLE 2

50 In this example, an active olefin polymerization catalyst was prepared by dissolving 1.2 g of bis(pentamethylcyclopentadienyl)zirconium dimethyl in 100 ml pentane and then adding dropwise 5 ml of a toluene solution containing 0.38 g of 7,8-dicarbaundecaborane(13). A bright yellow solid precipitated from solution. After thirty minutes, the solid was filtered off, washed with pentane and dried. The yield of product was 0.95 g. A portion of the product was analyzed and identified as bis(pentamethylcyclopentadienyl)methyl(dodecahydrido-7,8-dicarbaundecaborato) zirconium, the same active catalyst produced in Example 1.

#### EXAMPLE 3

60 In this example, an active olefin polymerization catalyst was prepared by dissolving 0.425 g of bis(ethyltetramethylcyclopentadienyl)zirconium dimethyl in 60 ml of pentane and adding dropwise 5 ml of a toluene solution containing 0.125 g of 7,8-dicarbaundecaborane(13). A bright yellow solid precipitated from solution. After fifteen minutes, the solid was filtered off, washed with pentane and dried. The yield of product was 0.502 g. A portion of the product was analyzed and identified as bis(ethyltetramethylcyclopentadienyl)methyl(dodecahydrido-7,8-dicarbaundecaborato)zirconium.

**EXAMPLE 4**

In this example, ethylene was polymerized using a portion of the catalyst produced in Example 2 by dissolving 50 mg of the catalyst in 100 ml of toluene and transferring the catalyst solution under a nitrogen atmosphere into a stirred, steel 1 liter autoclave which was previously flushed with nitrogen. The autoclave was pressured with 300 psig ethylene and stirred at 60°C. After thirty minutes, the reactor was vented and opened. The yield of linear polyethylene formed was 22.95 g.

**EXAMPLE 5**

In this example, ethylene was polymerized with the catalyst produced in Example 3 by dissolving 50 mg of the catalyst in 100 ml of toluene and transferring the catalyst solution under a nitrogen atmosphere into a stirred, steel 1 liter autoclave which was previously flushed with nitrogen. The autoclave was pressured with 400 psig ethylene and stirred at 40°C. After one hour, the reactor was vented and opened. The yield of linear polyethylene formed was 74.6 g.

**EXAMPLE 6**

In this example, ethylene was again polymerized with a portion of the catalyst produced in Example 2 by dissolving 75 mg of the catalyst in 100 ml of chlorobenzene and transferring under a nitrogen atmosphere into a stirred, steel 1 liter autoclave which was previously flushed with nitrogen. The autoclave was pressured with 150 psig ethylene and stirred at 40°C. After twenty minutes, the reactor was vented and opened. The yield of linear polyethylene formed was 3.3 g.

**EXAMPLE 7**

In this example, ethylene was polymerized with an active catalyst formed in situ by dissolving 80 mg of bis(pentamethylcyclopentadienyl)zirconium dimethyl and 35 mg of 1,2-dicarbaundecaborane(13) in 20 ml of dichloromethane. Ethylene was then bubbled through the solution at atmospheric conditions for one minute and the slurry then poured into an excess of ethanol. The polyethylene formed was filtered off, washed with water and acetone and dried. The yield of polyethylene was 1.6 g.

**EXAMPLE 8**

In this example, an active catalyst was prepared by reacting bis(pentamethylcyclopentadienyl)zirconium dimethyl (46 mg) with octadecaborane(22) (20 mg) in toluene (5 ml). There was considerable gas evolution. On passing ethylene through the solution for one minute, the solution grew hot. The vial was opened and acetone added to precipitate the polymer, which was filtered off, washed with acetone, and dried. The yield of polymer isolated was 0.32 g.

**EXAMPLE 9**

In this example, an active catalyst was prepared by reacting bis(pentamethylcyclopentadienyl)zirconium dimethyl (40 mg) with tri(n-butyl)ammonium tridecahydrido-7-carbaundecaborate (30 mg) in toluene (50 ml) in a serum-capped round-bottomed flask. The solution turned from colorless to orange-yellow. On passing ethylene through the solution for 1 minute, the solution grew hot as polymer precipitated from solution.

**EXAMPLE 10**

In this example, an active catalyst was prepared in an NMR tube by combining 50 mg of bis(pentamethylcyclopentadienyl) zirconium dimethyl and 40 mg of tri(n-butyl)ammonium 1-carbadodecaborate in 1 ml of hexadeuteriobenzene and placing the solution into the NMR tube. The disappearance of starting material was then observed by <sup>1</sup>H NMR spectroscopy and when the starting materials had disappeared ethylene was injected into the NMR tube. Solid polymer precipitated from the solution.

**EXAMPLE 11**

In this example, an active catalyst was again prepared in an NMR tube by dissolving 100 mg of bis[1,3-bis(trimethylsilyl) cyclopentadienyl]zirconium dimethyl and 60 mg of tri(n-butyl) ammonium 1-carbadodecaborate in 1 ml of hexadeuteriobenzene and then placing the solution into the NMR tube. The disappearance of starting materials was observed in the <sup>1</sup>H NMR spectrum. When all of the starting zirconium compound had disappeared, ethylene was injected into the tube and solid polymer precipitated from solution.

**EXAMPLE 12**

In this example, an active catalyst was again formed in an NMR tube by dissolving 100 mg of (pentamethylcyclopentadienyl) [1,3-bis(trimethylsilyl)cyclopentadienyl]zirconium dimethyl and 70 mg of tri(n-butyl)ammonium 1-carbadodecaborate in 1 ml of hexadeuteriobenzene and then placing the solution in the NMR tube. Disappearance of starting material was followed by <sup>1</sup>H NMR spectrum and when all of the starting zirconium compound had disappeared ethylene was injected into the tube. Solid ethylene polymer then precipitated from solution.

**EXAMPLE 13**

In this example, an active catalyst was prepared by suspending 80 mg bis(pentamethylcyclopentadienyl)zirconium dimethyl and 50 mg of bis[tri(n-butyl)ammonium]dodecaborate in 7 ml of toluene in a serum capped vial. On mixing, the suspension turned from colorless to yellow-green. Bubbling ethylene through the solution for 30 seconds caused a white polymer to form as the solution became warm. The vial was opened and the polymer precipitated with ethanol. The yield of polyethylene was 0.13 g.

**EXAMPLE 14**

In this example, an active catalyst was prepared by reacting bis(pentamethylcyclopentadienyl)zirconium dimethyl (45 mg) with tri(n-butyl)ammonium undecahydrido-1-carbaundecaborate (30 mg) in toluene (5 ml) in a serum-capped vial. The solution turned from colorless to yellow. On passing ethylene through the solution for 30 seconds, the solution grew hot as polymer precipitated.

**EXAMPLE 15**

In this example, an active catalyst was prepared by suspending 80 mg of bis(pentamethylcyclopentadienyl)zirconium dimethyl and 90 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III) in 5 ml of toluene in a serum-capped vial. The yellow solution turned orange-violet with gas evolution. On passing ethylene through the solution for 30 seconds, the solution turned deep violet with considerable evolution of heat and became viscous. The vial was opened and the solids precipitated with ethanol. These were washed with 10% aqueous sodium hydroxide solution, ethanol, acetone and hexane. The yield of polyethylene was 0.41 g.

**EXAMPLE 16**

In this example, an active catalyst was prepared by reacting bis(pentamethylcyclopentadienyl)zirconium dimethyl (40 mg) with N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)ferrate(III) (45 mg) in toluene (10 ml) in a serum-capped vial. On passing ethylene through the solution, the mixture grew hot as polymer formed. The vial was opened and the contents diluted with acetone, then filtered and dried. The yield of polymer isolated was 0.33 g.

**EXAMPLE 17**

In this example, an active catalyst was prepared by reacting bis(pentamethylcyclopentadienyl)zirconium dimethyl (40 mg) with tri(n-butyl)ammonium bis(7,8-dicarbaundecaborato)nickelate (III) (45 mg) in toluene (30 ml) in a serum-capped round-bottomed flask. Ethylene was passed through the solution for one minute. The solution grew hot as polymer precipitated from solution. The flask was opened and the contents diluted with acetone. The solid polymer was filtered off, washed with acetone and dried. The yield of isolated polymer was 0.48 g.

**EXAMPLE 18**

In this example, an active catalyst was prepared by suspending 100 mg of bis(methylcyclopentadienyl)zirconium dihydride and 180 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III) in 100 ml of toluene in a 250 ml round bottomed flask capped with a rubber septum. Ethylene was bubbled through the solution for 10 minutes. The flask was opened, the contents poured into hexane, filtered off and dried. The yield of polymer was 2.98 g.

**EXAMPLE 19**

In this example, an active catalyst was prepared by suspending 105 mg of bis[1,3-bis(trimethylsilyl)cyclopentadienyl]zirconium dimethyl and 90 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III) in 50 ml of toluene in a 100 ml round bottomed flask capped with a rubber septum. Ethylene was bubbled through the solution for 10 minutes. The flask was opened and the contents poured into ethanol and evaporated. The yield of polymer was 2.7 g.

**EXAMPLE 20**

In this example, an active catalyst was prepared by stirring 50 mg of bis(cyclopentadienyl)zirconium dimethyl and 90 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III) in 50 ml of toluene in a 100 ml round bottomed flask capped with a rubber septum. On passing ethylene through the solution, no obvious reaction was observed for one minute, after which a pronounced turbidity could be seen. After 10 minutes, the flask was opened, the contents diluted with ethanol and evaporated. The yield of polymer was 1.9 g.

**EXAMPLE 21**

In this example, ethylene was polymerized by reacting 69 mg of bis(cyclopentadienyl)hafnium dimethyl with 90 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III) in 50 ml of toluene in a septum-capped round bottomed flask. On passing ethylene through the solution, a pronounced turbidity appeared after 30 seconds as the solution grew hot. After 10 minutes, the solution was poured into acetone and the polymer filtered off and dried. The yield of linear polyethylene was 2.2 g.

**EXAMPLE 22**

In this example, ethylene was polymerized by reacting 50 mg of bis(trimethylsilylcyclopentadienyl)hafnium dimethyl with 45 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato) cobaltate(III) in 5 ml of toluene in a serum-capped vial. On passing ethylene through the solution, polymer formed as the mixture grew hot. After 1 minute, the vial was opened and the content diluted with acetone and filtered off. The yield of linear polyethylene was 0.35 g.

**EXAMPLE 23**

In this example, ethylene and 1-butene were copolymerized in a toluene diluent by adding under a nitrogen atmosphere to a 1 liter stainless-steel autoclave, previously flushed with nitrogen and containing 400 ml of dry, oxygen-free toluene, 35 ml of a toluene solution containing a catalyst prepared in situ from 50 mg of bis(cyclopentadienyl)zirconium dimethyl and 45 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III). 1-Butene (200 ml) was added to the autoclave, which was further pressurized with 120 psig of ethylene. The autoclave was stirred at 50° for 30 minutes, then cooled and vented. The contents were dried under a stream of air. The weight of the polymer isolated was 44.7 g. The melting point of the polymer was 117°C and analysis by infra-red spectroscopy indicated that there were about 17 ethyl branches per 1000 carbon atoms.

**EXAMPLE 24**

In this example, ethylene and 1-butene were copolymerized in a toluene diluent by adding under a nitrogen atmosphere to a 1 liter stainless-steel autoclave, previously flushed with nitrogen and containing 400 ml of dry, oxygen-free toluene, 50 ml of a catalyst solution in toluene containing 70 mg of bis(cyclopentadienyl)hafnium dimethyl and 45 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III). 1-Butene (200 ml) was added to the autoclave, which was further pressurized with 12- psig of ethylene. The autoclave was stirred at 50° for 20 minutes, then cooled and vented. The contents were dried under a stream of air. The yield of isolated polymer was 75.1 g. The melting point of the polymer was 109°C and analysis by infra-red spectroscopy indicated that there were about 29 ethyl branches per 1000 carbon atoms.

**EXAMPLE 25**

In this example, ethylene was polymerized by reacting 66 mg of 1-bis(cyclopentadienyl)titana-3-dimethylsila-cyclobutane and 88 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato) cobaltate(III) in 25 ml of toluene in a serum-capped round-bottomed flask. The solution darkened on passage of ethylene through it. After 10 minutes, the flask was opened and the contents diluted with ethanol. The polymer was filtered off, washed with ethanol and acetone, and dried. The yield of polyethylene isolated was 0.09 g.

**EXAMPLE 29**

In this example, ethylene was polymerized by reacting 61 mg of 1-bis(cyclopentadienyl)zircona-3-dimethyl-silacyclobutane and 87 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato) cobaltate(III) in 20 ml of toluene in a serum-capped round-bottomed flask. On passing ethylene through the solution, polymer precipitated as the solution grew warm. After 10 minutes, the vial was opened and the contents diluted with ethanol. The precipitate was filtered off, washed with ethanol, and dried. The yield of polyethylene isolated was 1.41 g.

**EXAMPLE 27**

In this example, ethylene was polymerized by reacting 82 mg of 1-bis(cyclopentadienyl)hafna-3-dimethylsila-cyclobutane and 88 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato) cobaltate(III) in 20 ml of toluene in a serum-capped round-bottomed flask. On passing ethylene through the solution, polymer precipitated as the solution grew hot. After 5 minutes, the flask was opened and the contents diluted with ethanol. The polymer was filtered off, washed with ethanol, and dried. The yield of polyethylene isolated was 1.54 g.

**EXAMPLE 28**

In this example, ethylene was polymerized by reacting 67 mg of bis(cyclopentadienyl)zirconium(2,3-dimethyl-1,3-butadiene) and 88 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato) cobaltate(III) in 50 ml of toluene in a serum-capped bottle. Ethylene was passed through the solution, which gradually grew warm. After 15 minutes, the bottle was opened and the contents diluted with ethanol. The polymer was filtered off, washed with ethanol, and dried. The yield of polymer isolated was 1.67 g.

**EXAMPLE 29**

In this example, ethylene was polymerized by reacting 40 mg of bis(cyclopentadienyl)hafnium(2,3-dimethyl-1,3-butadiene) with 43 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato) cobaltate(III) in 50 ml of toluene in a serum-capped bottle. Ethylene was passed through the solution, which became turbid within 30 seconds. After 20 minutes, the bottle was opened and the contents diluted with ethanol. The solid polymer was filtered off, washed with ethanol, and dried. The yield of polyethylene isolated was 0.43 g.

**EXAMPLE 30**

In this example, ethylene was polymerized by reacting 55 mg of (pentamethylcyclopentadienyl)(tetramethyl-  
 eta<sup>1</sup>-methylene -eta<sup>6</sup>-cyclopentadienyl)zirconium phenyl and 45 mg of N,N-dimethylanilinium bis(7,8-dicar-  
 baundecaborato)cobaltate(III) in 20 ml of toluene in a serum-capped round-bottomed flask. On passing  
 5 ethylene through the solution, polymer formed almost instantly and much heat was evolved. After 5 minutes,  
 the flask was opened and the contents diluted with ethanol. The precipitate was filtered off, washed with  
 acetone, and dried. The yield of polyethylene isolated was 0.55 g.

**EXAMPLE 31**

In this example, ethylene was polymerized by reacting 80 mg of (pentamethylcyclopentadienyl)(tetramethyl-  
 cyclopentadienylmethylene)hafnium benzyl and 60 mg of N,N-dimethylanilinium bis(7,8-dicarbaundecabor-  
 ato)cobaltate(III) in 50 ml of toluene in a serum-capped bottle. Ethylene was passed through the solution for 10  
 minutes. Polymer precipitated as the solution grew warm. The bottle was opened and the contents diluted with  
 15 ethanol. The solid polymer was filtered off, washed with acetone, and dried. The yield of polyethylene isolated  
 was 0.92 g.

**EXAMPLE 32**

In this example, ethylene was polymerized by reacting 0.42 g of bis(trimethylsilylcyclopentadienyl)hafnium  
 dimethyl with 0.08 g N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)cobaltate(III) in 10 ml of toluene. A  
 20 portion of this solution (0.4 ml) was injected under a pressure of 3000 bar of Isopar into an autoclave  
 pressurized to 1500 bar with ethylene and heated to 160°. After 5 seconds the contents of the autoclave were  
 discharged. Linear polyethylene (2.1 g) with a weight-average molecular weight of 144,000 and a molecular  
 weight distribution of 2.9 was isolated.

While the present invention has been described and illustrated by reference to particular embodiments  
 thereof, it will be appreciated by those of ordinary skill in the art that the same lends itself to variations not  
 necessarily illustrated herein. For this reason, then, reference should be made solely to the appended claims for  
 purposes of determining the true scope of the present invention.

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**Claims**

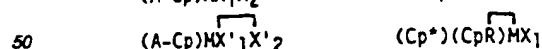
1. Method for preparing a catalyst comprising the steps of:

35 (a) combining, in a suitable solvent or diluent, at least one first compound consisting of a  
 bis(cyclopentadienyl)metal compound containing at least one substituent capable of reacting with a  
 proton, said metal being selected from the group consisting of titanium, zirconium and hafnium and  
 at least one second compound comprising a cation, capable of donating a proton, and an anion  
 containing a plurality of boron atoms which is bulky, labile and capable of stabilizing the metal cation  
 40 formed as a result of the reaction between the two compounds;

(b) maintaining the contacting in step (a) for a sufficient period of time to permit the proton  
 provided by the cation of said second compound to react with said substituent contained in said  
 metal compound; and

45 (c) recovering an active catalyst as a direct product or as a decomposition product of one or more  
 of said direct products from Step (b).

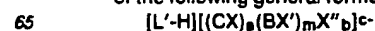
2. Method according to Claim 1 wherein said bis(cyclopentadienyl)metal compound may be  
 represented by the following general formulae:



Wherein:

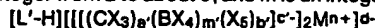
M is a metal selected from the group consisting of titanium (Ti), zirconium (Zr) and hafnium (Hf); (A-Cp) is  
 either (Cp)(Cp\*) or CP-A'-CP\* and Cp and Cp\* are the same or different substituted or unsubstituted  
 55 cyclopentadienyl radicals, optionally two independently substituted or unsubstituted radicals; A' is a  
 covalent bridging group containing a Group IV-A element; L is an olefin, diolefin or aryne ligand; X<sub>1</sub> and X<sub>2</sub>  
 are, independently, selected from the group consisting of hydride radicals, hydrocarbyl radicals,  
 substituted-hydrocarbyl radicals, optionally two lower alkyl substituents or two hydrides, organo-metal-  
 loid radicals and the like; X'<sub>1</sub> and X'<sub>2</sub> are joined and bound to the metal atom to form a metallacycle, in  
 60 which the metal, X'<sub>1</sub> and X'<sub>2</sub> form a hydrocarbocyclic ring containing from about 3 to about 20 carbon  
 atoms; and R is a substituent on one of the cyclopentadienyl radicals which is also bound to the metal  
 atom.

3. Method according to Claim 1 or Claim 2 wherein said second compound may be represented by one  
 of the following general formulae:



Wherein:

L'-H is either H<sup>+</sup>, ammonium or a substituted ammonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical, a phosphonium or substituted-phosphonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical and the like; B and C are, respectively, boron and carbon; X, X' and X'' are radicals selected, independently, from the group consisting of hydride radicals, halide radicals, hydrocarbyl radicals, organo-metalloid radicals and the like; a and b are integers  $\geq 0$ ; c is an integer  $\geq 1$ ; a + b + c = an even-numbered integer from 2 to about 8; and m is an integer ranging from 5 to about 22; and/or

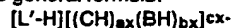


Wherein:

L'-H is either H<sup>+</sup>, ammonium or a substituted ammonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical, a phosphonium or substituted-phosphonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical and the like; B, C, M and H are, respectively, boron, carbon, a transition metal and hydrogen; X<sub>3</sub>, X<sub>4</sub> and X<sub>6</sub> are radicals selected, independently, from the group consisting of hydride radicals, halide radicals, hydrocarbyl radicals, organo-metalloid radicals and the like; a' and b' are the same or a different integer  $\geq 0$ ; c' is an integer  $\geq 2$ ; a + b' + c' = an even-numbered integer from 4 to about 8; m' is an integer from 6 to about 12; n is an integer such that 2c' - n = d; and d is an integer  $\geq 1$ .

4. Method according to any of the preceding claims wherein the contacting of step (a) is accomplished at a temperature within the range from about -100° C to about 300° C, preferably at from 0 to 45,000 psig.

5. Method according to any of the preceding claims wherein said second compound is represented by the general formula:

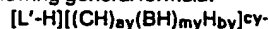


Wherein:

L'-H is either H<sup>+</sup>, ammonium or a substituted-ammonium optionally tri-substituted radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical, a phosphonium or substituted-phosphonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical and the like; B, C, and H are, respectively, boron, carbon and hydrogen; ax is either 0 or 1; cx is either 2 or 1; ax + cx = 2; and bx is an integer ranging from 10 to 12.

6. Method according to Claim 6 wherein said second compound is selected from the group consisting of bis[tri(n-butyl) ammonium] dodecaborate and tri(n-butyl)ammonium 1-carbaundeca or 1-carbadodecaborate and said first compound is selected from the group consisting of bis(pentamethylcyclopentadienyl)zirconium dimethyl, (pentamethylcyclopentadienyl) (cyclopentadienyl)zirconium dimethyl, and [1,3-bis(trimethylsilyl)cyclopentadienyl]zirconium dimethyl.

7. Method according to any of Claims 1 to 4 wherein said second compound is represented by the following general formula:

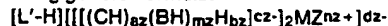


Wherein:

L'-H is either H<sup>+</sup>, ammonium or a substituted-ammonium, optionally tri-substituted, radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical, a phosphonium or substituted-phosphonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical and the like; B, C and H are, respectively, boron, carbon and hydrogen; ay is an integer from 0 to 2; by is an integer from 0 to 3; cy is an integer from 0 to 3; ay + by + cy = 4; and mx is an integer from 9 to 18.

8. Method according to Claim 7 wherein said second compound is selected from the group consisting of tri(n-butyl) ammonium 7,8-dicarbaundecaborate and tri(n-butyl)ammonium tridecahydrido-7-carbaundecaborate in which case preferably the first compound is bis(pentamethylcyclopentadienyl)zirconium dimethyl and/or wherein L'-H is H<sup>+</sup>, preferably 7,8-dicarbaundecaborane(13) or octadecaborane(22) in which case optionally said first compound is selected from the group consisting of bis(pentamethylcyclopentadienyl)zirconium dimethyl and bis(ethyltetramethylcyclopentadienyl)zirconium dimethyl.

9. Method according to any of Claims 1 to 4 wherein said second compound may be represented by the following general formula:



wherein:

L'-H is either H<sup>+</sup>, ammonium or a substituted ammonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical, a phosphonium or substituted-phosphonium radical having up to 3 hydrogen atoms replaced with a hydrocarbyl or substituted-hydrocarbyl radical and the like; B, C, H and MZ are, respectively, boron, carbon, hydrogen and a transition metal; az is an integer from 0 to 2; bz is an integer from 0 to 2; cz is either 2 or 3; mz is an integer from 9 to 11; az + bz + cz = 4; and nz and dz are, respectively, 2 & 2 or 3 & 1.

10. Method according to Claim 9 wherein said second compound is N,N-dimethylanilinium bis(undecahydrido-7,8-dicarbaundecaborato) cobaltate(III) and/or wherein said first compound is selected from the groups consisting of 1-bis(cyclopentadienyl)titanla-3-dimethylsilacyclobutane, 1-bis(cyclopentadienyl)zirconia-3-dimethylsilacyclobutane, and 1-bis(cyclopentadienyl)hafna-3-dimethylsilacyclobutane, bis(cyclopentadienyl) zirconium (2,3-dimethyl-1,3-butadiene) and bis(cyclopentadienyl)

hafnium(2,3-dimethyl)-1,3-butadiene), (pentamethylcyclopentadienyl) (tetramethylcyclopentadienylmethylene)zirconium phenyl and (pentamethylcyclopentadienyl) (tetramethylcyclopentadienylmethylene)hafnium benzyl; or wherein said second compound is selected from the group consisting of N,N-dimethylanilinium bis(7,8-dicarbaundecaborato)nickelate(III) and N,N-dimethylanilinium bis(7,8-ditadienyl)zirconium dimethyl.

11. Method for polymerizing an  $\alpha$ -olefin, a diolefin and/or an acetylenically unsaturated compound containing from 2 to about 18 carbon atoms either alone or in combination with one or more other monomers comprising the steps of:

(a) contacting at a temperature within the range from about  $-100^{\circ}\text{C}$  to about  $300^{\circ}\text{C}$  and at a pressure within the range from about 0 to about 45,000 psig. an olefin, diolefin and/or an acetylenically unsaturated monomer either alone or in combination with one or more other monomers in a suitable carrier, solvent or diluent with a catalyst prepared previously or in situ during polymerization by a method according to any of the preceding claims;

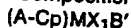
(b) continuing the contacting of step (a) for a sufficient period of time to polymerize at least a portion of said olefin;

(c) recovering a polymer product.

12. A catalyst prepared by a method according to any of Claims 1 to 10.

13. Polyolefin produced in accordance with the method of claim 11.

14. Composition of matter containing compounds represented by the following general formula:



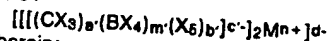
Wherein:

M is a metal selected from the group consisting of titanium (Ti), zirconium (Zr) and hafnium (Hf); (A-Cp) is either (Cp)(Cp\*) or CP-A'-Cp\* and Cp and Cp\* are the same or different substituted or unsubstituted cyclopentadienyl radicals; A' is a covalent bridging group containing a Group IV-A element; X<sub>1</sub> is selected from the group consisting of hydride radicals, hydrocarbyl radicals, organo-metalloid radicals and the like; and B' is a compatible non-coordinating anion which may be represented by one of the following general formulae:



wherein:

B and C are, respectively, boron and carbon; X and X' and X'' are radicals selected, independently, from the group consisting of hydride radicals, halide radicals, hydrocarbyl radicals, organo-metalloid radicals and the like; a and b are integers  $\geq 0$ ; c is an integer  $\geq 1$ ; a + b + c = an even-numbered integer from 2 to about 8; and m is an integer ranging from 5 to about 22; and 34



Wherein:

B, C and M are, respectively, boron, carbon and a transition metal; X<sub>3</sub>, X<sub>4</sub> and X<sub>5</sub> are radicals selected, independently, from the group consisting of hydride radicals, halide radicals, hydrocarbyl radicals, organo-metalloid radicals and the like; A' and b' are the same or a different integer  $\geq 0$ ; C' is an integer  $\geq 2$ ; a' + b' + c' = an even-numbered integer from 4 to about 8; m' is an integer from 6 to about 12; n is an integer such that  $2c' - n = d$ ; and d is an integer  $\geq 1$ .

15. Composition of matter according to Claim 14 wherein (A-Cp) is a bis(peralkyl-substituted cyclopentadienyl); X is an alkyl group; B' is (dodecahydrido-7,8-dicarbaundecaborato) and M is zirconium and wherein each of the alkyl groups in the peralkyl-substituted cyclopentadienyl radicals are, independently, C<sub>1</sub>-C<sub>20</sub> alkyl radicals and the alkyl group is a C<sub>1</sub>-C<sub>20</sub> alkyl radical, the peralkyl substitution being preferably pentamethyl or ethyltetramethyl and the alkyl radical being preferably a methyl radical.





European Patent  
Office

# EUROPEAN SEARCH REPORT

Application Number

EP 88 30 0698

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 4)
D,A	JOURNAL OF THE CHEMICAL SOCIETY, CHEMICAL COMMUNICATIONS, 1986, pages 1610-1611; M. BOCHMANN et al.: "Synthesis and insertion reactions of cationic alkylbis(cyclopentadienyl)titanium complexes" * Whole abstract *	1	C 08 F 4/64 C 08 F 4/76 C 08 F 10/00 C 07 F 17/00
D,A	EP-A-0 200 351 (MITSUI PETROCHEM) * Whole document *	1	
A	US-A-3 231 593 (W. HAFNER et al.) * Claims; column 5, line 71 - column 6, line 7; examples *	1	
			TECHNICAL FIELDS SEARCHED (Int. Cl. 4)
			C 08 F C 07 F
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 14-04-1988	Examiner DE ROECK R.G.
CATEGORY OF CITED DOCUMENTS			
<p>X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document</p> <p>T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons &amp; : member of the same patent family, corresponding document</p>			

FORM 1503 (12/82) (FPOB)